

## BINDALS PAPERS MILLS LIMITE

Paper Unit & Head Office: 8th Km, Bhopa Road, Muzaffarnagar-251 001 (U.P.), INDIA Sugar & Distillery Unit: Vill, Changipur, Tehsil Chandpur, Distt. Bijnor-246734 (U.P.) Regd. Office: NP-151 B, Maurya Enclave, Pitampura, Delhi - 110 088, INDIA

CIN: U21011DL2006PLC148926 | GSTIN: 09AADCB0282B1Z6

Ref: Bindal/SD/EHS/2024-25/15

Date: 29.09.2025

To, The Chief Environmental Officer (Circle-7) Utter Pradesh Pollution Control Board TC-12V, Vibhuti Khand, Gomti Nagar Lucknow-226010

Sub: Environmental Statement of BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION) Village - Changipur, Block - Noorpur, Tehsil -Chandpur, Distt - Bijnor, Uttar Pradesh-246734

Dear Sir,

Please find attached herewith environmental statement of BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION) Village - Changipur, Block - Noorpur, Tehsil - Chandpur, Distt - Bijnor, Uttar Pradesh for the financial year ending on 31st March, 2025.

Thanking You,

Yours faithfully

For BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION) Village - Changipur Distt - Bijnor, Uttar Pradesh

Authorized S

C.C.: Regional officer, U.P. Pollution Control Board, Bijnor

Encl.: As Above

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#### **ENVIRONMENTAL STATEMENT**

OF

## BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION) VILLAGE - CHANGIPUR, DISTRICT- BIJNOR (U.P.)

(SUGAR UNIT)

FINANCIAL YEAR ENDING THE 31<sup>ST</sup> MARCH, 2025



#### PREPARED BY:

BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION)
VILLAGE - CHANGIPUR, DISTRICT- BIJNOR (U.P.

#### (FORM - V) (See Rule 14)

Environmental Statement Report for the Financial Year ending the 31st March, 2024.

#### PART - A

(i)	Name and address of the	BINDALS PAPERS MILLS LIMITED
	Owner/occupier of the Industry	(SUGAR & DISTILLERY UNIT) Village
	operation or process	- Changipur, Block - Noorpur, Tehsil -
(ii)		Chandpur, Distt – Bijnor, Uttar Pradesh
(ii)	Production Capacity	SUGAR UNIT -10000 TCD
(iii)	Year of Establishment	2023
(iv)	Date of Last environmental statement submitted	
(v)	Industry category	
	Primary : (STC Code)	Secondary
	Secondary : (SIC Code)	Secondary

# PART – B Water and Raw Material Consumption 2024-25

(I) TOTAL WATER CONSUMPTION : 261 M³/Day

a) Process : 236
b) Cooling : 00
c) Domestic : 25

Name of Products Process water consumption per unit of output

During the Previous
Financial Year
(2023-24)

During the current
Financial Year
(2024-25)

Plantation white Sugar 0.620 0.437

1 fort

## (II) Raw Material Consumption RAW MATERIAL CONSUMED AND PRODUCT AT A GLANCE

Crushing season (2024-25)

Particulars	2024-25	2023-24
Date of start of plant	04 November 2024	04 November 2023
Date of Finish		AL CONTROL DESIGNATION OF THE PARTY OF THE P
Gross season days	15 March 2025	21 March 2024
Duration of season days	132	139
Total Car	131.15	118.39
Total Cane crushed (T)	800864.311	558958.226
Total sugar made (T)	78727	57530
Total Molasses made (T)	40720	33873.29
Total Bagasse produced (T)	215284.80	150806.929
Total Filter cake produced (T)	31028.68	20457.871
Lime Consumed (T)	1449.0	1067.61
Sulphur consumed (T) Oil & Grease consumed (T)	455.30	370.43
Caustic soda consumed (T)	7.27	229.17
Washing soda consumed (T)	11.13	1419.75
Total Raw Sugar Melt (T)	1.0	55.90
The Cagai Meit (1)	NA	NA

S. N.	Name of Raw Material	Name of Products	Consumption of Raw		
			During the previous Financial Year 2023 – 2024	During the Current Financial Year 2024 - 2025	
1	Sugar Cane	Sugar	9.72		
2.	1 ima		9.72	10.17	
۷.	Lime	Sugar	0.0186	0.01840	
3.	Sulphar	Sugar	0.0053	0,01040	
		ougu,	0.0053	0.005783	
4.	Caustic Soda	Sugar	0.0247	0.000141	
5.	Washing Soda	Sugar	0.0010	0.000141	
	Washing Soda	Sugar	0.0010	0.00001270	
6.	Phosphoric Acid	Sugar	0.0041		
			ein as Anneyura No. 4	0.0172	

\* Season 2024-25 RT 8C is enclosed herein as Annexure No. 1.

#### PART - C

#### Pollution discharged to Environment / unit of output:

Sugar ETP Treated Water flow 1.84 M³/MT of sugar 0.180 M³/MT of Cane

(1)	Pollution	Quantity of Pollutants discharged. (Mass / day)	Concentrations of pollutants in discharges (Mass / Volume)	Percentage of variation from Prescribed standards
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#### (a) WATER

Sugar Unit:

Average Flow	828.03 M³/day	07.0 M-#:	
Suspended Solids	5.796 Kg/Day	07.0 Mg/Liter	86.00 % lower
B.O.D	10.764 Kg/Day	13.0 Mg/Liter	87.00 % lower
C.O.D.	59.616 Kg/day	72.00 Mg/Liter	71.20 % lower

Third party sugar ETP treated water analysis report is attached as Annexure No.2

#### (b) AIR:

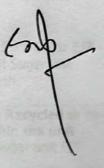
Sugar Unit:

100 TPH stack 31 mg/NM3

38 % lower

Third party sugar unit boiler Stack Emission analysis report is attached as annexure No.3

Ambient air monitoring report is attached herein as annexure No.4
Noise monitoring report is also thatched herein as Annexure No.5.



#### Part -D

#### **HAZARDOUS WASTES**

(As specified under hazardous wastes/management and handling rules, 2016)

Па	zardous wastes	Total Quantity (MT)		
		During the Previous Financial year 2023-24	During the current Financial yea 2024-25	
<ul> <li>a) From pollution control facilities (Waste oil and grease is collected in Sheetla waste Management.)</li> </ul>				
Ha	zardous waste disposal form 10 is	attached herein as Anne	xure No. 6.	
		PART -E	Delet as self-	
	SOLI	D WASTE		
		Tota	l Quantity (MT)	
(a)	From Process	During the previous financial year 2023-24	During the current financial year 2024-25	
	(i) Filter cake	20457.871	31028.68	
(b)	From Pollution Control Facilities			
	(i) Sludge from Sugar ETP (ii) 100 TPH Sugar unit Boiler ash.	500 1650.35	700 2746.56	
C. Haz Formac Derreta	(1) Quantity Recycled or re- utilized within the unit Sludge from Sugar unit ETP	100% as manure	100% as manure	
(c)	(2) Sold:			
	(3) Disposed	NA	NA	
	(i) Filter Cake (ii) 100 TPH Sugar unit Boiler ash.	20457.871 1650.35	31028.68 2746.56	

\*Filter cake MT: Filter cake provided to farmer for using as manufacture.

\*Ash disposed off environment friendly on low laying land.

#### Part -F

Please specify the characterization (in terms of composition and quantum) of hazardous as well as solid wastes and indicate disposal practice adopted for both these categories of wastes.

(a) Filter cake: -Lighter than soil.

Sp. Gravity (approx.) 1.29

Bulk density 0.70 gm/cc(approx.)

Constituents: -Carbon 34 % .

Nitrogen 1.63 %.

Phosphate 2.52 %.

Potash 0.55 %.

Calcium, Iron, Manganese, Zinc 4.74 %

pH 6.8 to 7.0

Quantum: -20457.871 MT.

Disposal: -Filter cake provided to farmer for using as manure.

Boiler ash:

Constituents Calcium 5.33 %.

Aluminum 16.37 %.

Combustible matter .40 %.

Disposal: Ash collected from E.S.P and disposed off environment friendly on low laying land. The suppression of ash is being done by the water spraying from sprinkling system. Finally soil is put above the ash up to 1  $\frac{1}{2}$  fits.

Quantum 1650.35 MT

(C) Hazardous Waste:

From pollution control facilities -Waste oil and used grease

Quantum:-860 Kg.

Constituants :-Physical form- Liquid & semi solid.

> Percentage solid -5 %. Chemical composition -N.A.

oil and Disposal:- Waste grease collected from the machines /oil and grease trap in PVC drums, and send to the TSDF M/s

Waste management projects ltd.

## Impact of the pollution abatement measures taken on conservation of natural resources and on the cost of production.

- Closed loop cold and hot water recirculation system.
- CPU is installed for recycle the water.
- 3. Anaerobic treatment is added for the strengthen of effluent treatment and the quality of final treated effluent.
- 4. ETP Treated water gainfully used in ferti-irrigation by local farmers and in our own
- 5. Solid waste management in environment friendly manner.
- 6. Reduction in air pollution and water pollution by efficient operation of pollution control devices operation.

#### PART - H

## Additional measures/investment proposal for environmental protection including abatement of pollution, prevention of pollution.

- 1. 20000 Nos tree plantations & promotion of greenery on a large scale in surrounding areas of factory and nearby villages.
- 2. Diffused aeration system is adopted.
- Online Continuous Emission Monitoring System is installed at stack of Boiler. 3.
- Telemetry piezometer system is installed.
- 5. Flow meters installed at various point of water consumption for reducing the water consumption as well as reducing the waste water generation.
- 6. Extra oil skimmer is installed at mill house outlet for proper separation of oil and grease from mill house drain.

#### **Treatment Strategy of Effluent:**

#### SUGAR ETP TREATMENT SCHEME

Bindals Papers Mills Ltd. established its sugar unit in 2023, and as part of this setup, they also incorporated advanced technology for their effluent treatment plant (ETP). This move reflects a commitment to sustainability and environmental responsibility.

By using advanced treatment technologies, Bindals Papers Mills Ltd. ensures that the effluent produced during the sugar production process is adequately treated, the release of pollutants such as organic matter, chemicals, and suspended solids into the environment within the prescribed limits. This not only helps in compliance with environmental regulations but also supports sustainable practices in the sugar industry. Advanced ETP technologies typically employ a combination of physical, chemical, and biological processes to remove contaminants from effluent.

#### **ETP PROCESS:**

The waste water collected from mill house, boiling house and power house is collected in collection pit through RCC drain and transfer through pipe line to the E.T.P. The treatment process is following

#### 1. Process effluent:

- I. Primary Treatment: It consists mainly physical and chemical treatment.
  - a. Bar Screen: A coarse screen is fixed in the drain before the equalization tank of E.T.P. for the removal of coarse material / particles such as paper, cloth etc.
  - b. Oil skimmer: The effluent passes through a fixed type mechanical oil skimmer for the removal of oil and grease from the surface of effluents. The oil & grease collected is scrapped from the surface & is stored in a PVC drum. The same is being sent to authorize TSDF.
  - c. Equalization tank: The effluent now enters into Equalization tank to homogenize the waste water. The Equalization tank provides the necessary retention time for mixing of varying Effluents so as to attain the average value for the various parameters.
- d. **Flash Mixer:** The effluent now enters into a reaction / flash mixing tank; here the effluent is mixed thoroughly with the requisite doses of lime and polyelectrolyte's by with stirring. The pH of the resulting effluent should be 7.5 to 8 to at this stage.

e. **Primary clarifier:** The mixed effluent is then fed into a primary clarifier at a definite rate with the help of a centrifugal pump. The mixed effluent is then fed into a central flocculation chamber cum feed channel and the annular settling chamber. This is fitted with the low speed paddle mixer for flock formation. This flocculated solid mass settles on the bottom floor, from where it is continuously swept into bottom sludge well by mechanical scrapper for eventual removal into sludge drying bed under hydrostatic head.

The addition of lime and polyelectrolyte helps in coagulating most of the colloidal solid as well as all suspended solids and their eventual removal. The settled sludge at the bottom of the clarifier is collected in sludge well by means of rotating mechanical system. From here the sludge is removed by a sludge pump and sent to sludge drying bed.

2. Spray Pond Effluent: The spray pond effluent received from the cooling of PAN in process house, it contains mainly sulphar pollutant load and some organic pollutant load.

#### I. Primary treatment:

- a. Equalization tank: The spray pond effluent directly received through pipe line in Equalization tank to homogenize the waste water. The Equalization tank provides the necessary retention time for mixing of varying Effluents so as to attain the average value for the various parameters. The mixing in carried out by the coarse diffuser aertion.
- b. Flash Mixer: The effluent now enters into a reaction / flash mixing tank; here the effluent is mixed thoroughly with the requisite doses of lime and polyelectrolyte's by with stirring. The pH of the resulting effluent should be 10 to 10 at this stage.
- c. Primary clarifier: The mixed effluent is then fed into a primary clarifier at a definite rate with the help of a centrifugal pump. The mixed effluent is then fed into a central flocculation chamber cum feed channel and the annular settling chamber. This is fitted with the low speed paddle mixer for flock formation.
- d. Lime (Calcium Hydroxide): This is added to the water to increase the pH, which causes the precipitation. In this case, the lime helps in the precipitation of sulfur in the form of calcium sulfate (gypsum). Polyelectrolyte aids in the coagulation process by promoting the aggregation of small colloidal particles into larger flocs, making it easier to remove suspended solids. Precipitation and Coagulation reacts to form calcium sulfate (CaSO<sub>4</sub>), which precipitates out of the water.

Polyelectrolyte helps in coagulating the colloidal solids, causing them to clump together and settle out of the water more effectively. This flocculated solid mass settles on the bottom floor, from where it is continuously swept into bottom sludge well by mechanical scrapper for eventual removal into sludge drying bed under hydrostatic head.

# II. Secondary Treatment:

- a. Common collection Tank: The clarified water is being collected in the common collection tank from the both clarifier and transferred to the buffer tank of anaerobic treatment through pipe line
- b. Buffer Tank: The buffer tank is being used for the preparation of effluent to feed in the ICX anaerobic reactor by adding the nutrient as required caustic, DAP, Urea and micronutrient.
- c. Anaerobic Treatment: In the BIOPAQ ICX reactor uses anaerobic granular biomass converts Bio degradable organic components (COD) from wastewater into biogas. The generated biogas is separated from the treated wastewater and collected in the gas holder. After the biological process is completed, the treated waste water overflow sends to aeration tank for further treatment. Anaerobic wastewater treatment is a type of biological treatment where anaerobic microorganisms are used to break down and remove organic contaminants from wastewater in absence of oxygen.
- d. Gas holder and flare stack: The generated biogas collected in gas holder and being flared through the stack. This system is in auto mode.
- e. Aerobic Treatment: The anaerobic treated effluent feed in the aerobic treatment. Aeration in an activated sludge process is based on pumping air into a tank, which promotes the microbial growth in the wastewater. Aeration provides oxygen to bacteria for treating and stabilizing the wastewater. Oxygen is needed by the bacteria to allow biodegradation to occur. The supplied oxygen is utilized by bacteria in the wastewater to break down the organic matter containing carbon to form carbon dioxide and water.

The excess sludge produced during the bio-oxidation process is discharged in sludge drying bed for dewatering. A high sludge concentration (MLSS) of 2500-3000mg/ltr is maintained within the system.

f. Secondary Clarifier: The activated sludge process is based on the recycle sludge mass from the secondary settler. Sludge is recycling into the aeration chamber to maintain high sludge concentration. The excess sludge produced during the biooxidation process is discharged in sludge drying bed for dewatering.

#### 3. Excess condensate Effluent:

- a. Neutralization tank: In this tank the excess condensate is being taken from UGR and the pH is being corrected up to 7-7.5 by the dosing of caustic.
- b. Aerobic Treatment: The neutralization tank effluent feed in the aerobic treatment. Aeration in an activated sludge process is based on pumping air into a tank, which promotes the microbial growth in the wastewater. Aeration provides oxygen to bacteria for treating and stabilizing the wastewater. Oxygen is needed by the bacteria to allow biodegradation to occur. The supplied oxygen is utilized by bacteria in the wastewater to break down the organic matter containing carbon to form carbon dioxide and water. The excess sludge produced during the bio-oxidation process is discharged in sludge drying bed for dewatering. A low sludge concentration (MLSS) of 1000-1500mg/ltr is maintained within the system as the COD load of the condensate is very low up to 500 mg/lit.
- c. Tube settler: The aerated effluent is being entered in the tube settler by gravity and the supernatant further feed to HRSCC.
- d. High Rate Solid Contact Clarifier (HRSCC): The supernatant tube settler water is being feed in HRSCC with flocculent dosing for further cleaning of the colloidal solids.
- e. Sludge Drying Bed: The sludge drying bed is made off bed with pebbles and coarse sand which is provide the filtration of water and the solids parts of sludge collected on the surface of beds.
- III. Tertiary treatment: The HRSCC supernatant liquid is stored in the tank. The effluent from collection tank is pumped into coarse sand filter & activated carbon filter respectively. Both units are in series and they not only reduce suspended solids to a great extent but also help in removing of B.O.D. to some extent.
- IV. UF Filtration: The liquid (typically water) is forced through the ultra filtration membrane under pressure. Permeate (clean water or filtered liquid) passes through the membrane, while the larger particles and contaminants are retained and form the concentrate which is typically sent for further treatment in aeration tank. The UF

water is being utilized in distillery cooling tower makeup and RO feed water for makeup water of boiler.

V. Reverse Osmosis (RO): RO is a membrane filtration process that removes contaminants from water by applying pressure to force water through a semi-permeable membrane, leaving behind dissolved solids, microorganisms, and other contaminants. The RO water is being recycled to feed water for boller operation, Process Flow diagram of ETP is attached herein as Annexure No. 7.

Sanitary and domestic disposal: - The domestic and sanitary effluent is being treated in sewage treatment plant and will be totally utilized in horticulture as per the norms of UPPCB.

The STP treated water analysis report is attached herein as Annexure No. 8.

P refins alun

# Any other particular for improving the quality of the environment.

- 1. Awareness program of farmer by Agriculture scientist.
- 2. We have installed modern plant in keeping view of minimum steam consumption, minimum fresh water consumption by adopting the best available recycle, reduce
- 3. Farmer Awareness tour for new technique in agriculture.
- 4. HDPE Pipe line up to 5.0 km to farmer field irrigation.
- 5. Regular monitoring of noise level, waste and stack gasses being done as per the schedule given below in the crushing season.

Process/Unit Frequency		Sampling points to be analyzed	Parameters of sampling	
1.	Screen	fluent treatment plant		
	Screen	Outlet & inlet Floating material	Hourly	
2.	Oil & Grease trap			
3.	Equalization tank	Outlet & inlet oil & grease	Twice in shift	
4.	Primary clarifier	Outlet pH, S.S	Hourly	
5.		Outlet SS	Daily-once	
	Diffused Aeration Tank	MLSS, pH, DO	Shift wise	
6.	Final clarifier	Outlet BOD,COD, S.S, pH	Real Time	
Air I	Pollution Control Device		redi Time	
	Wet scrubber.	Stack SPM	Pool Time	
Nois	se Level Monitoring		Real Time	
1.	Near the plant			
	recar the plant	Noise level	Weekly	





# BINDALS PAPERS MILLS LIMITED

UNIT- SUGAR CHANGIPUR, BIJNOR (U.P.)

FINAL MANUFACTURING REPORT RT-8(C) Season: 2024-25



Cheporate Office: Bindals Papers Mills Limited 8th Km., Bhopa Road Muzaffarnagar -251001, UP, India Ph:+91-131-2468381, 9917055355 Email:info@bindalpapers.com

ess of Factory : eration No. of Factory :- 69067 rocess used >

FORM R. T. B (C)
(For Central Super Factories)
Final Manufacturing Report for Season 2024-25

(Central Excise Rule 83)

Bindals Papers Mills Ltd (Unit-Sugar &Distillery Division) Changipur Bijnor ( U.P)
Div.: Moradabad Range: Bijnor

Charme	ation Process used : Double Sulp	hitation Process		
E NO.	PARTICULAR	\$	This Season	Last Seaso
	Time Account		2024-25	2023-2
	Date of start		Charles of the Control of the Contro	
	Time of start		04-Nov-24	04-Nov-3
	Date of finish		6:15 PM	7:15 P
	Time of finish		15-March-2025	21-March-202
	Gross Season		11:45 PM	11:05 P
	Duration of season -	days	132	13
	Total hours Actual Crushing	days	131.15	118.3
	Total hours lost	(Hrs)	2885.35	2604.
	i ) Cane shortage	(Hrs)	264.15	711.
	ii ) Mechanical and Electrical	(Hrs)	190.97	612.
	iii ) Process	(Hrs)	51.64	64.
	iv ) General cleaning	(Hrs)	0.00	0.
	W / General Cleaning		21.54	19.
	v )Growers & Truck Strike	(Hrs)	0.00	0.0
113	v ) Misc (Inclement weather+Festivals etc.)	(Hrs)	0.00	15.
		(Hrs)		
	Cane Crushed:		DE CONTRACTOR DE	
	i ) Own Estate Cane		0.00	0.0
	ii ) Gate Cane	Qtis.	3772661.22	4127241.
6.9	iii ) Out Station (centre) Cane	Qtds.		1462340.
	iv) Total	Qtts.	4235981.89	5589582.
		Qtis.	8008643.11	
3	Juice & Added Water			
	Average Gross Mixed Juice % Came		113.75	117.
	Correction % Mixed juice		0.44	0.
324	Average Net Mixed juice % Cane		113.25	116.
	Total Net Mixed juice	Qtls.	9069677	65352
	Average Added Water	% Cane	40.63	44.
4	Sugars	Ne Garre	Sign of the same o	THE RESERVE
	Total Sugar bagged			
	i) No. of bags a) 50 kg	Nos.	1574540.00	1150600.
		Nos.	0.00	0.
	b) 100 kg	Qtis.	787270*	575300
	ii ) Total Quantity Bagged	Otis.	0.00	0.
	Sugar in Process , if any		787270.00	575300.
	Total Sugar made	Qtts.	0.00	0.
	Sugar recovered from previous season's process	Qtis.	0.00	0.
	Sugar recovered from pre. season's remelt sugar	Qtis.	0.00	
	Sugar recovered from Raw Sugar	Qtis.	787270*	0.
	Total net Sugar made	Qtls.	191210	57530
5	Molasses		407200.00	
	Total Molasses sent out	Qtls.		338732.
	Molasses in process ,if any	Qtis.	0.00	0.
	Droduced	Qtis.	407200.00	338732.
	from previous season's process	Qtis.	0.00	0.
	Molasses recovered from pre. season's remelt sugar	Qtis.	0.00	0.
	Molasses recovered from Raw Sugar	Qtis.	0.00	0.
	Total net Molasses made This Includes 2350 Qtls. BISS (Brown Sugar) of above 9		407200.00	338732.



	PARTICULARS	This Season 2024-25	Last Seaso 2023-2
6 Recovery			2023-2
Average Recovery of at	Igar percent cane	9.83	10.2
	final molasses percent cane	5.08	6.0
7 Bagasse percent Cane	Section 1. The Reput of the Section 1.	26.88	26.9
8 Filter cake percent can	O THE RESERVE OF THE PARTY OF T	3.87	3.6
9 Stores used			
Bagasse percent cane			
a) Trial	% Cane	0.019	0.89
b) Season c) Season (RDF)	% Cane	12.830	20.03
Lime a) Process	% Cane Qtis. Per 100 Qtis.of cane	2.045	
b) ETP	Qtis. Per 100 Qtis.of cane	0.178	0.17
c) Coolin		0.000	0.02
Sulphur	Qtis. Per 100 Qtis.of cane	0.057	0.05
Phosphoric Acid	Kg per 100 Qtls.of Cane	0.017	0.04
Color PPt (for Juice)	Kg per 100 Qtls.of Cane	0.047	0.02
Color PPt (For melt)	Kg per 100 Qtls.of Cane		
Lubricants	Ltrs. Per 100 Qtls.of Cane	0.052	0.02
Grease	Kg per 100 Qtis.of Cane	0.038	0.01
Seed Slurry Biocides	Kg per 100 Qtis.of Cane Kg per 100 Qtis.of Cane	0.140	0.07
Washing soda	Kg per 100 Qtls.of Cane	0.051	0.06
Caustic soda (Process)	Kg per 100 Qtls.of Cane	0.125	0.01
Caustic soda (Boller)	Kg per 100 Qtls.of Cane	0.013	0.21
Viscosity reducer	Kg per 100 Qtls.of Cane	0.041	0.03
Flocculant (Juice)	Kg per 100 Qtls.of Cane	0.016	0.02
Flocculant (Melt)	Kg per 100 Qtls.of Cane		
Dextranase	Kg per 100 Qtls.of Cane	0.0130	0.007
Alpha-amylase Scale softner	Kg per 100 Qtis.of Cane Kg per 100 Qtis.of Cane	0.0210	0.019
Antifoam	Kg per 100 Qtls.of Cane	0.0370 0.0210	0.059
Bleaching Powder	Kg per 100 Qtis.of Cane		0.017
Boiler Chemicals	Kg per 100 Qtis.of Cane	0.0420	0.022
Eloguard	Kg per 100 Qtls.of Cane		Section 19 as
Comman Salt	Kg per 100 Qtls.of Cane		
Hydrochloric Acid	Kg per 100 Qtls.of Cane	0.020	0.07
10 ANALYSIS			
Cane	Sugar percent	11.79	13.2
	Fibre percent	13.11	12.8
Primary juice	Sugar percent	14.14	15,4
	Brix percent Purity	17.33 81.59	18,0
Mixed Juice	Sugar percent	10.05	83,;
	Brix percent	12.54	10.9
The Contract of Participation	Purity	80.16	81,1
Last Express juice	Sugar percent	1.30	1.3
Security Sections	Brix percent	1.75	2.:
Clarified juice	Purity	74.29	74.1
Clarified Juice	Sugar percent Brix percent	9.52 11.80	10.4
	Purity	80.68	12.0
Un Sulphured Syrup	Sugar percent	55.17	82.4 54.1
	Brix percent	69.18	66.1
	Purity	79.75	82.0
Sulphured Syrup	Sugar percent	54.92	54.
	Brix percent Purity	68.99	66.
Massecuite	City	79.61	81.1
Masseculte -A	Brix percent		
	Purity	91.17 90.42	88.0
Masseculte -A1	Brix percent	91.62	89.:
	Purity	79.73	90.4
Masseculte -B	Brix percent	93.00	90.8
The second for the	Purity - Section 1	73.41	75.1
Masseculte -C	Brix percent	97.21	95.1
Massecuite -C1	Purity	61.08	57.0
massocuite -C1	Brix percent	92.94	Ltd. (Un
	Purity	68.44	119

100

Vill Grangpur (Distr. hiptor (U.P.)

VO.		PARTICULARS	This Season	Last Seaso
	Molasses	[17] [1] [1] [1] [1] [1] [1] [1] [1] [1] [1	2024-25	2023-2
	A - Heavy			
		Brix percent	77.92	***
	A - Light	Purity	76.75	74.9
		Brix percent	67.02	76.7
	A1 - Heavy	Purity	92.30	64.7
1	ni - rieavy	Brix percent	80.64	90.9
	9 11	Purity		79.2
	B - Heavy	Brix percent	59.12	64.1
		Purity	82.58	81.2
	C1 - Heavy	Brix percent	49.56	53.8
		Purity	85.07	
	C- Light		48.02	
		Brix percent	75.54	74.13
		Purity	70.53	71.61
	Sugar			
	White Sugar (Bagged)	Sugar percent		
			99.90	99.90
	C-Heavy Molasses	Moisture percent	0.027	0.028
		Sugar percent	26.57	37.75
		Brix percent	85.25	83.26
	Bagasse	Purity	31.17	45.34
		Sugar percent	1.52	1.77
		Moisture percent	49.17	50.11
	Filter cake	Fibre percent	48.78	47.52
	I Have been been a second	Sugar percent	1.57	1.67
1	Mill Extraction, Boiling House Ex	traction & Overall Extraction		
	Imili Extraction	addition a Overall Extraction		
	Reduced Mill Extraction (deer)		96.55	96.41
	Boiling House Extraction		96.73	96.50
	Reduced Boiling House Extraction		86.29	80.51
	Overall Extraction		89.76	84.51
	Reduced Overall Extraction		83.29	77.6
1	2 SUGAR BALANCE		86.82	81.2
	Sugar in Cane			
	Sugar in Mixed Juice		11.79	13.2
	Sugar in Bagasse		11.38	12.7
	Sugar in Filter Cake		0.41	0.4
	Sugar in Final Molasses		0.06	0.0
	Sugar in sugar		1.35	2.2
	Sugar undetermined		9.82	10.2
			0.15	0.1
	Total Losses (in Bagasse, Filter cake, declare that the figures given in this	Molasses & Undetermined)	1.97	2.9

I hereby declare that the figures given in this return are complete and true to the best of my knowledge and belief.

Date :

(Neeraj Sharma) Mgr. (QC)

(Shashi Gupta )
President (Sugar & Distillery)

ed. (Unit

Note: a) Sugar means "direct Pol"

b) Bagasse percent cane= 100 + Added water % cane - Mixed Juice (Gross) % cane

c) Gross season means total No. of days from the date of start to the date of close, both days inclusive.

d) Duration of season : Days calculated by dividing the total actual crushing hours by 22 .

e) Out station cane is the cane weighed and purchased at a centre other than the factrory

los

#### BINDALS PAPERS MILLS LIMITED UNIT -SUGAR ADDITIONAL INFORMATIONS ALONG WITH FINAL MANUFACTURING REPORT

No.		PARTICULARS		This Season 2024-25	Last Season 2023-24
1	Mill Extraction			96.55	96,40
2	Reduced Mill Extraction	in		90.05	
	а) Deerr				96.50
	b) Reduced Extraction	- (Allerati		96.73	96.28
				96.71	80.58
				86.29	60.56
28	Reduced Boiling Hou	se Extraction			84,21
	a) Gundu Rao			89.38	
	b) Noel Deerr			89.76	84.58 77.68
	5 Overall Extraction			83.29	17.08
	6 Reduced Overall Extra	action			
	a) Gundu Rao			86.46	81.26
	b) Noel Deerr			86.82	81.62
	7 Undiluted juice lost %		Halland Life	24.25	25.23
	8 Added water extracte	d in mixed juice % adde	ed water	77.04	73.72
	9 Added water % fibre			309.88	346.32
	10 DMF			72.62	72.52
	11 Java Ratio			83.28	85.71
	12 Crush rate (MT) per 2	24 hours			
	a ) Including Stoppa			6103	4046
	b) Excluding stopp			6662	5150
	c) Sanctioned Cape			8500	8500
	13 Capacity Utilization	Distriction of the Control of the Co		71.80	47.60
		- Net		78.38	60.59
	14 Total Time lost % Av	vailable		8.39	21.45 40.01
	15 Steam consumption			32.17	40.01
	16 E.R.Q.V.				96.49
	a) M.J./ P.J.			96.56	80.52
	b) L.M.J./ P.J.			82.45	42.18
	17 Power Consumptio	n (KWH/Ton of Cane)		36.72	72.10
	18 Massecuite % Cane			60.50	25.20
	a) A- Massecuite			28.50 2.50	3.34
	b) A1-Massecuit			12.50	14.85
	c) B- Massecuite			7.30	8.07
	d) C- Massecuite			2.00	•
	e) C1- Massecuite			52.80	51.45
	f) Total Massecuite	9 %			
700	22 Gradewise sugar p	roduction (Qtls.) This Season:	2024.25	Last Season : 2023	3-24
			%ge	QUANTITY	%ge
	ISS GRADE	QUANTITY	0.02	4055	0.70
	LI-30	125	7.02	57785	10.04
	L-31	55240	75.59	375505	65.27
	M-31	595075	0.15	14515	2.52
	M-30	1150 132730	16.86	107540	18.69
	S-31	600	0.08	14400	2.50
	S-30	2350	0.30	1500	0.26
	BISS	787270	100.00	575300	100.00

Mr. Shashi Gupta

TOTAL

- President (Sugar & Distillery Division)

Mr. Mukesh Mittal

- Sr.Vice President (Technical)

Mr. Jitendra Malik

- Vice President (Cane)

Mr. Pawan Kr Gupta

- Dy. General Manager (Production)

Mr. Neeraj Shrma

Manager (QC)

787270



## **Newcon Consultants & Laboro**



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#### TEST REPORT

Page No.: 1 of 1

TEST REPORT No. NCL/EP-047/30/11/24

DATE OF REPORT: 04/12/2024

Name and Address of Customer

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changlpur, District - Bijnor

SAMPLING DETAILS

Sample Name

: EFFLUENT WATER

Analysis Start Date

. 30/11/2024

Analysis End Date

: 04/12/2024

Date of Sampling

: 29/11/2024

Sample ID No.

NCL/EP-047/30/11/24

Time of Sampling

. 10:00 AM

Sample Receipt Date

: 30/11/2024

Sampling Done By

: NCL

Environmental Condition: 27±2°C

Sampling Description Sampling Location

: EFFLUENT WATER AFTER TREATMENT

: ETP OUTLET

Sample Quantity

: 2 Ltr

Sampling Protocol

: IS: 17614 (P-1)

Packing

: PVC BOTTLE

**Packing Condition** 

: Sealed

#### **TEST RESULT**

S.No.	Test Parameters	Unit	Test Method	Results	Specification As per CPCB (Sugar Industry)
1	рН	-	IS: 3025 (P-11)	7.27	5.5-9.0
2	Total Suspended Solids (TSS)	mg/L	IS: 3025 (P-17)	7.0	100
3	Bio Chemical Oxygen Demand (3 Days at 27°C)	mg/L	IS: 3025 (P-44)	13	30
4	Chemical Oxygen Demand (COD)	mg/L	APHA-5220 B	72	250
5	Oil & Grease	mg/L	IS: 3025 (P-39)	1.4	10

\*\*\*End of Report\*\*\*

EP-047/30/11/24-1

exection Incharge

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FOR NEWCON CONSULTANTS & LABORATORIES

Authorized Signato

Laboratory: A-1/156, Sector-17, (Swadeshi Compound) Kavi Nagar Industrial Area, GHAZIABAD - 201 002 (U.P.)

Mobile: 9810430345, 9205501788 | Website: www.newconlab.in E-mail: newconlab@gmail.com, newconlabfinance@gmail.com



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TEST REPORT

mexure No.3

Page No.: 1 of 1

TEST REPORT No. NCL/EP-087/11/12/24

**DATE OF REPORT : 16/12/2024** 

Name and Address of Customer

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changipur, District - Bijnor

SAMPLING DETAIL

Sample Name

: STACK EMISSION

**Analysis Start Date** Date of Sampling

Sampling Protocol

Sampling Location

**Equipments Used** 

: 11/12/2024

: 10/12/2024

: AS PER CPCB GUIDELINES

Sample ID No.

Vayubodhan Stack Sampler No-1

VSS-1 (S.No-321 DTC 01)

DETAILS OF STACK

Stack Attached to Type of fuel used : Boller

: Bagasse

Stack height above the ground : 72.0 Mtr

Stack dia at the top Attached APCS

: ESP

: 20°C

: 2500 mm

Capacity

Quantity of fuel used

Analysis End Date

Sampling Done By

Area Category

**Duration of Sampling** 

Stack height above the roof top Material of Construction

Normal Oprating Schedule

Sampling Flow Rate of SPM

: AS PER REQUIREMENT

Comminssioning date

**Ambient Temperature** 

PHYSICAL OBSERVATIONS

Flue gas temperature

: 98°C : 25.0 LPM

: 18/12/2024

: 30 Minutes

: 100 TPH

: 34 MT/DAY

: NCL/EP-087/11/12/24

: NCL

: 7.5 Mtr/sec Velocity of the flue gases Sampling Flow Rate for Gases : 2.4 LPM

Quantity of Emission discharged: 103803.38 Nm³/hr

TEST RESULT

S.No.	Test Parameters	Units	Test Method	Results	Specification As Per CPCB
	Particulate Matters (PM)	mg/Nm³	IS:11255 (Part-1)	. 34	250
	r divosition memory	mg/Nm³	IS:11255 (Part-2)	13	Not Specified
	Odipilot Divisio	%	18:13270	0.042	Not Specified
	Odiodii ilia	mg/Nm³	IS:11255 (Part-7)	47	Not Specified
4	Oxide of Nitrogen (NOx)	MA ASSESSED TO	-J-10	Section 18 to 18	

EP-087/11/12/24-1



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TEST REPORT

Amexure No. 4

Page No.: 1 of 2

TEST REPORT No. NCL/ED-013/28/02/25

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Name and Address of Customer

Village - Changipur, District - Bijnor

SAMPLING DETAIL

Sample Name

: AMBIENT AIR

28/02/2025

**Analysis End Date** 

: 03/03/2025

**Analysis Start Date** Date of Sampling

: 27/02/2025

Sampling Done By

: NCL

10:00 AM (27/02) TO 10:00 AM (28/02) Sampling Location

· Near Boiler Area

Time of Sampling Sampling Protocol

: IS:5182

Sample ID No.

· NCL/ED-013/28/02/25

**DATE OF REPORT: 03/03/2025** 

Sampling Flow Rate of SPM : 1.27 Mtr3/min

Sampling Flow Rate for: 0.5 LPM

(Average)

Gases

: 24 Hrs

Sampling Machine Placed at : 3.0 Mtr Height (from ground)

Sampling Duration **Equipments Used** 

: Respirable Dust Sampler (PM10)+Fine Particulate Sampler (PM2.5) With Gaseous Attachment

PHYSICAL OBSERVATIONS Wind Direction

: East to West

Ambient Temperature

: 27°C

Weather Conditions

: Clear

#### TEST RESULT

S.No.	Test Parameters	Units	Test Method	Results	Specification As per CPCB
1	Particulate Matters (Size Less Than 10µm) (PM10)	µg/m3	IS:5182 (Part 23)	84	For 24 Hrs=100
2	Particulate Matters (Size Less Than 2.5µm) (PM2.5)	μg/m3	NCL/AIR/STP-09	45	For 24 Hrs=60
3	Sulphur Dioxide (SO2)	µg/m3	IS:5182 (Part 2)	18.1	For 24 Hrs=80
4	Carbon Monoxide (CO)	mg/m3	IS:5182 (Part 10)	0.64	For 08 Hrs=02 For 1 Hrs =04
5	Nitrogen Dioxide (NO2)	µg/m3	IS:5182 (Part 6)	32.2	For 24 Hrs=80
6	Lead (Pb)	µg/m3	IS:5182 (Part 22)	BDL(DL-0.05)	For 24 Hrs=1.0
7	Ozone (O3)	µg/m3	IS:5182 (Part-9)	20.8	For 8 Hrs=100 For 1 Hr=180
8	Ammonia (NH3)	µg/m3	NCL/AIR/STP-13	BDL(DL-20.0)	For 24 Hrs=400
9	Benzene (C6 H6)	µg/m3	IS:5182 (Part-11)	BDL(DL-1.0)	For Annual=05
10	Benzo (a) Pyrene (BaP)	ng/m3	IS:5182 (Part-12)	BDL(DL-0.1)	For Annual=01

ED-013/28/02/25-1

charge Checked by

FOR NEWCON CONSULTANTS & LABORATORIES

Co Lab Head

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Page No.: 2 of 2

TEST REPORT No. NCL/ED-013/28/02/25

DATE OF REPORT :03/03/2025

S.No.	Test Parameters	Units	Test Method	Results	Specification As
11	Arsenic (As)	ng/m3	NCL/AIR/STP-19	BDL(DL-1.0)	For Annual=06
12	Nickel (Ni)	ng/m3	NCL/AIR/STP-17	BDL(DL-5.0)	For Annual=20

\*\*\*End of Report\*\*\*

Remarks: BDL=Below Detection Limit.

ED-013/28/02/25-2



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#### TEST REPORT

Page No.: 1 of 2

TEST REPORT No. NCL/ED-014/28/02/25

DATE OF REPORT: 03/03/2025

Name and Address of Customer

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changipur, District - Bijnor

#### SAMPLING DETAIL

Sample Name

: AMBIENT AIR

: 28/02/2025

**Analysis End Date** 

: 03/03/2025

**Analysis Start Date** 

Sampling Done By

· NCL

**Date of Sampling** Time of Sampling 27/02/2025 10:00 AM (27/02) TO 10:00 AM (28/02)

Sampling Location

: Near Stockyard

Sampling Protocol

: IS:5182

Sample ID No.

: NCL/ED-014/28/02/25

Sampling Flow Rate for : 0.5 LPM

(Average)

Sampling Flow Rate of SPM : 1,26 Mtr³/min

Gases

Sampling Machine Placed at : 3.0 Mtr Height (from ground)

Sampling Duration

. 24 Hrs

: Respirable Dust Sampler (PM10)+Fine Particulate Sampler (PM2.5) With Gaseous Attachment

**Equipments Used** 

: 27°C

Wind Direction

: East to West

**Ambient Temperature** Weather Conditions

: Clear

#### **TEST RESULT**

PHYSICAL OBSERVATIONS

S.No.	Test Parameters	Units	Test Method	Results	Specification As per CPCB
1	Particulate Matters (Size Less Than 10µm) (PM10)	µg/m3	IS:5182 (Part 23)	80	For 24 Hrs=100
2	Particulate Matters (Size Less Than 2.5µm) (PM2.5)	µg/m3	NCL/AIR/STP-09	42	For 24 Hrs=60
3	Sulphur Dioxide (SO2)	µg/m3	IS:5182 (Part 2)	17.6	For 24 Hrs=80
4	Carbon Monoxide (CO)	mg/m3	IS:5182 (Part 10)	0.61	For 08 Hrs=02 For 1 Hrs =04
5	Nitrogen Dioxide (NO2)	µg/m3	IS:5182 (Part 6)	31.4	For 24 Hrs=80
6	Lead (Pb)	µg/m3	IS:5182 (Part 22)	BDL(DL-0.05)	For 24 Hrs=1.0
7	Ozone (O3)	µg/m3	IS:5182 (Part-9)	20.5	For 8 Hrs=100 For 1 Hr=180
8	Ammonia (NH3)	µg/m3	NCL/AIR/STP-13	BDL(DL-20.0)	For 24 Hrs=400
9	Benzene (C6 H6)	µg/m3	IS:5182 (Part-11) 5098	BDL(DL-1.0)	For Annual=05
10	Benzo (a) Pyrene (BaP)	ng/m3	IS:5182 (Part-12)	BDL(DL-0.1)	For Annual=01



Duig Authorized Signatory d

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Page No.: 2 of 2

TEST REPORT No. NCL/ED-014/28/02/25

**DATE OF REPORT: 03/03/2025** 

S.No.	Test Parameters	Units	Test Method	Results	Specification As per CPCB
11	Arsenic (As)	ng/m3	NCL/AIR/STP-19	BDL(DL-1.0)	For Annual=06
12	Nickel (Ni)	ng/m3	NCL/AIR/STP-17	BDL(DL-5.0)	For Annual=20

\*\*\*End of Report\*\*\*

Remarks: BDL=Below Detection Limit.

ED-014/28/02/25-2

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#### TEST REPORT

Page No.: 1 of 1

TEST REPORT No. NCL/ED-015/28/02/25

Name and Address of Customer

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changipur, District - Bijnor

SAMPLING DETAIL

Sample Name Analysis Start Date

**Date of Monitoring** 

: Ambient Noise

28/02/2025

27/02/2025

24 Hrs

**Analysis End Date** 

· NCL . Monitoring Done By

Place of Monitoring

: Near Boiler Area

: 28/02/2025

DATE OF REPORT : 03/03/2025

Time of Monitoring

**Monitoring Duration** 

10:30 AM (27/02) TO 10:30 AM (28/02)

Protocol

: NCL/AIR/STP/20

Category of Area

: Industrial Area

**OBSERVATIONS** 

Observation No.	1	2	3	4	5	6	7	8	9	10
Day Time Reading (dB(A)	62.8	63.3	63.9	64.2	64.5	65.1	65.6	66.2	66.7	67.
Night Time Reading (dB(A)	52.7	53.2	53.8	54.3	54.9	55.2	55.6	56.1	56.7	57.

#### **TEST RESULT**

S.No	Test Parameter	Results	Specification As Per CPCE
Day	Time Noise Level		
1	Average Noise Level	- 65.0	
2	L Max	67.4	
3	L Min	62.8	
4	Day Leq	65.2	75.0 Max
Nigh	t Time Noise Level		
5	Average Noise Level	55.0	
5	L Max	57.2	
7	L Min	52.7	
3	Night Leq	55.2	70.0 Max

\*\*\*End of Report\*\*\*

Remarks: >Day time reckoned between 6:00AM To 10:00PM. >Night time reckoned between 10:00PM To 06:00AM.

ED-015/28/02/25-1

DRIVEWEDIN CONSOLIANTS & LABORATORIES

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TEST REPORT

SAMPLING DETAIL

Page No.: 1 of 1

TEST REPORT No. NCL/ED-016/28/02/25 Name and Address of Customer

DATE OF REPORT : 03/03/2025

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT) Village - Changipur, District - Bijnor

Sample Name

: Ambient Noise

Analysis Start Date Date of Monitoring

28/02/2025

Monitoring Duration : 24 Hrs

: 27/02/2025

Analysis End Date Monitoring Done By

: NCL : Near Stockyard

Place of Monitoring

Time of Monitoring Category of Area

: 10:30 AM (27/02) TO 10:30 AM (28/02) : Industrial Area

Protocol

: NCL/AIR/STP/20

: 28/02/2025

Observation No.	11	2	3	4	5	6	7	-	67.7	68.1
Day Time Reading (dB(A)	63.6	64.1	64.5	65.3	65.9	66.2	66.7	67.2		57.6
Night Time Reading (dB(A)	52.8	53.4	54.1	54.7	55.3	55.9	56.2	56.8	57.1	

#### TEST DESIII T

		TEST RESULT	Specification As Per CPCB
S.No	Test Parameter	Results	Specification
	Time Noise Level		
1	Average Noise Level	65.9	
_		68.1	
2	L Max	63.6	
3	L Min	66,1	75.0 Max
4	Day Leq		the same of the sa
liah	Time Noise Level		
	Average Noise Level	55.4	
	L Max	57.6	
		52.8	
	L Min	55.6	70.0 Max
	Night Leq	**** J of Poport***	

\*\*\*End of Report\*\*

Remarks: >Day time reckoned between 6:00AM To 10:00PM.

>Night time reckoned between 10:00PM To 06:00AM.

ED-016/28/02/25-1

OR NEWCON.CONSULTANTS & LABORATORIES

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FORM 10 [See rule 19 (1)] Amexuse No-6

S. No. HW

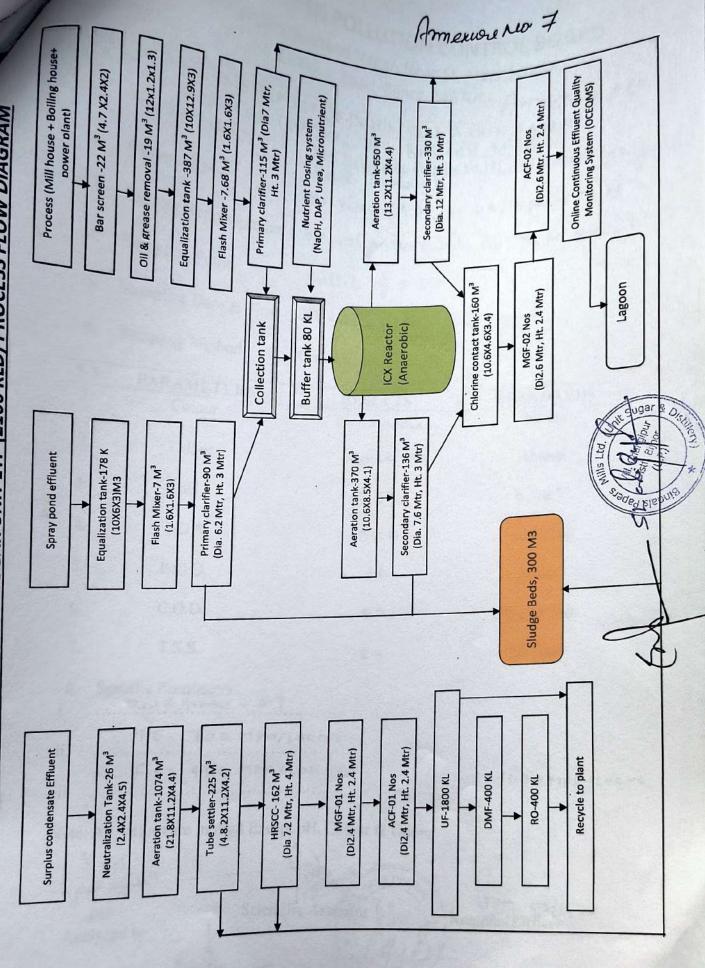
11916

# MANIFEST FOR HAZARDOUS AND OTHER WASTE

To Be Forwarded By The Sender To The State Pollution Control

		Danud Africa	ed By The Sender To The State Pollution Com ning All The Seven Copies
	Name and Mai	ling Address	45
	Main Name and Main No. and Main	d E-mail) :	Changiour.
	sender's Authorisation N	lo.:	Binge (II P) /8
19	Manifest Document No.	( ) ( ) ( ) ( ) ( ) ( ) ( ) ( ) ( ) ( )	11919 1919 1919 19025
IN	ransporter's Name and	Address	Midals Palm
1	including Phone No. and	d E-mail) :	S. W. M. (P
ti	Type of Vehicle:		(Truck/Tanker/Special_Vehicle)
1	Transporter's Registratio	n No. :	19-169T-0849
	Vehicle Registration No.		DY - 164 1 - DO IFCT
	Receiver's Name and Mailing Address (including Phone No. and E-mail):	D-26 & 37, UPSIDC Industrial Dist. Bulandshahr, Uttar Prade	SII - 200200 accom
+	Receiver's 13443 U	PPCB/Bulandshahar(UPPCBRO)	/HWM/ BULANDSHAHAR/2023   Date - 2000
9.	Authorisation No.: 18353570	JPPCB/Bulandshanar(UFFCBRC	/HWM/ BULAND SHAHAR/2020   Dated: 08/01/2023 P/CTO/both/BULANDSHAHAR/2023   Date: 20/05/2023 Oly Sludge U.
10.	Waste Description		Nos
11.	Total Quantity		
-	No. of Containers :		(Solid/Semi-Solid/Sludger Sny)
12.	Physical Form:		
13.	Special Handling Instruct	tions and Addition	point of leadin spillage proof container
	Information:		any malerial mondare that the contents
10	. Sender's Certificate		the consignment are fully and by
14	. Sender's Certificate		accurately described and are
(2)			proper simprio
		Trit Sugar & Oit	categorised, packed, marked, in led, and are in all respects in led, and are for transport by
		Drive San Stell	led, and are in all respect by proper conditions for transport by road according to applicable national road according to applicable national
			road according to appropriate regulations.
		( ) 10 11	Day Month
	Name and Stamp: S	Signature red supplied	29092029
	J. J. day	ement of Receipt of	
1	5. Transporter Acknowledge Sheetala Waste N		Day Month Year
-	Wastes Add Das to	DOING IN THE TOTAL	-10 0 0 9 5
1	Name and Standard, Bulan GSTIN-09AD 16. Receiver's certification for	SFS73 of hazardous	and other waste
	16. Receiver's certification is	Signature:	Day Month Year

# BINDALS PAPERS MILLS LTD. SUGAR UNIT ETP (2100 KLD) PROCESS FLOW DIAGRAM



# UTTAR PRADESH POLLUTION CONTROL BOARD

Maharshi Dayanand Nagar, Near St. Mery School, Chakkar Road, Bijnor-246701

mexure No. O ANALYSIS REPORT OF INDUSTRIAL WASTE WATER

Sample Code: UPPCB/R.L./W.W./BPS-08 /2024

Name of Industry

: M/s Birdals Paper Mills Htd vill chargeper

Ristl-Bynor.

2. Collected by :Mr vipy (RO), Mr S.K Tripathi CS.A)

Factory Representative : Mr. salyender kuman Giri (0 9 M E H S)

Sampling Point : outlet of s. T. P

Sampling Date & Time : 21 | 11 | 2024 , 12:30 PM 5.

Sampling Method 6. : Grab

S.N	PARAMETERS	RESULTS	STANDARDS
1.	Colour	Cotourters	Absent
2.	Odour	odourless	Absent
3.	pH	7.83	6.5-8.5
4.	T.D.S.	520	1600/2100
5.	B.O.D.	14	20/30
6.	C.O.D.	40	50/150/250
7.	T.S.S.	25	30/100
8. i.	Specific Parameters	>7	TANK CONTRACTORS
ii.	T.C. 700 MI	h/100 mt	
iii.	F.C- 460 MI		1000 MPH/100m

Note: All Values are in mg/l Except pH, Colour & Odour

Analyzed by

Scientific Assistant

Regional Offi

# ENVIRONMENTAL STATEMENT

OF

BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION)
VILLAGE - CHANGIPUR, DISTRICT- BIJNOR (U.P.)

(DISTILLERY UNIT)

FINANCIAL YEAR ENDING THE 31<sup>ST</sup> MARCH, 2025



#### PREPARED BY:

BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION)
VILLAGE - CHANGIPUR, DISTRICT- BIJNOR (U.P.

# Environmental statement for the financial year ending the 31st March, 2025

#### Part -A

(1) Name and Address of the Owner /occupier of the industry, operation or process.

: BINDALS PAPERS MILLS LIMITED (SUGAR & DISTILLERY DIVISION) VILLAGE - CHANGIPUR, DISTRICT- BIJNOR (U.P.)

(ii) Industry Category Primary : (SIC Code) Secondary: (SIC Code)

: Distillery

(iii) Production Capacity (units)

: 150 KLD (Rectified Spirit / Ethanol / Absolute Alcohol)

: 2023 (iv) Year of Establishment

(v) Date of the last environmental : 30.09.2024 Statement submitted

#### PART - B

# Water and Raw Material Consumption 2024-25

: 188 M³/day 1) TOTAL WATER CONSUMPTION

a) Process : 188 M³/day

b) Cooling

: 00 Sugar ETP treated water is being used

: 00 c) Domestic

#### Name of Products

## Process water consumption per unit of output

Rectified Spirit / A.A /Ethanol

During the Previous Financial Year (2023-24)

During the current Financial Year (2024-25)

2.14 KL/ KL gugar &

1.84 KL/KL

#### 2) RAW MATERIAL CONSUMPTION Name of raw material Consumption of raw material per unit of output During the current Financial year During the previous (2024-25) Financial year (2023-24)4.237 MT /KL OF AA

----

#### PART C

3.8 MT /KL OF AA

# Pollution discharged to envi

(1) Pollutants	god to environment/unit of output:						
	pollutants discharged (mass/day)	Concentration of pollutants in discharged (mass / volume)	Percentage of variation from prescribed standards with reasons				
a) Water:	Not Applicable (It's a Zero liquid discharge Industry)						
b) Air:		na/Nm3	38% lower				

Third party distillery unit boiler Stack Emission analysis report is attached as annexure No.1.

Ambient air monitoring report is attached herein as annexure No.2 Noise monitoring report is also thatched herein as **Annexure No. 3.** 

#### PART - D

#### **Hazardous Wastes**

(As specified under the Hazardous Waste (Management, Handling and Transboundary Movement Rules, 2016)

riazardous wastes	Total Quantity (Kg.)				
Turmer for eachy in services	During the previous - Financial year (2023-24)	During the current Financial year (2024-25)			
(a) From Process	NIL	NIL			
(b) From pollution control facilities	NIL	NIL			

#### PART - E

#### SOLID WASTE

#### **Total Quantity (MT)**

		Ouring the previous Financial year 2023-2024	During the current Financial year 2024-2025
(a)	From Process  (i) Fermenter sludge from Distillery unit	597	952
(b)	From Pollution Control Facilities	and the first of the second	
	(i) 25 TPH Distillery unit incineration boiler ash	2786.69	5300
	(1) Quantity Recycled or re utilized within the unit	NA NA	8 Ing unit (CSQ) 1
(c)	(2) Sold: 25 TPH Incineration Boiler Ash	1546.70	3741
	(3) Disposed		
	(i) Fermenter sludge from Distillery unit	597	952
ARRIVAN MENINT	(ii) 25 TPH Distillery unit incineration boiler ash	1240	1559

\*Fermenter sludge provided to farmers for using as manure.

\*Incineration boiler ash sold to M/s Ram Potash 3741 MT and balance ash provided to

farmer for using as manure

Please specify the PART - F

adopted for both indus as mall mastes and indicate disposal quantum) of hazardous as well as solid wastes and indicate disposal adopted for both these categories of waste.

Constituents

: Not Applicable

Disposal

: Not Applicable

Mode of Disposal

: Not Applicable

: Not Applicable

Impact of the pollution abatement measures taken on conservation of natural resources PART - G natural resources and on the cost of production.

- 1. Total spent wash gainfully utilized in incineration boiler as a fuel.
- 2. We have made the spent wash lagoon by RCC to ensure no leakage. 3. Both lagoons RCC is protected by FRP based epoxy coating material.
- 4. The Process generated condensate treated in condensate polishing unit (CPU) & gainfully recycled in the process to conserve the ground water resource.
- 5. The sugar unit treated effluent utilized in distillery unit to conserve the ground water.

#### PART - H

Additional measures / investment proposal for environmental protection including abatement of pollution prevention.

- 1. We carried out regular monitoring of air, water and noise as per specified guidelines is being carried out.
- We have installed the online continuous emission monitoring system.
- 3. We have installed the mass flow meters on the MEE inlet and MEE outlet.
- 4. We carried out the Occupational Health Surveillance programme is being organized and the record of the same is being kept accordingly.
- 5. For proper disposal and make sure the Zero liquid discharge the company has installed and efficiently operated the incineration belief

Any other particulars for improving the quality of the environment.

The unit is working The unit is committed to zero effluent discharge for which it is working for maximum resource to zero effluent discharge for which it is working for maximum resource in the committed to zero effluent discharge for which it is working for maximum resource. maximum resource conservation. Since this distillery is a recent installation, action for further. action for further improving the quality of environment has been planned in the following areas:

- Water conservation by reuse/ recycling of different streams of water.

  Occurred ii) Occupational Health Surveillance and monitoring according to laid down parameters under Factories Act and to take corrective action in case of deviations.
- iii) We have installed the full fledged fire fighting system including fire hydrants, water sprinkler system and foam flooding system.





Ameque 210.1

# UTTAR PRADESH POLLUTION CONTROL BOARD

Maharshi Dayanand Nagar, Near St. Merry School, Bijnor

Ref No. 29095397/Bijnore/2024

Stack Emission Test Report

Date: 27/11/2024

2.

3-

Name & Address of Industry: Bindals paper mills Ltd. Vill- Changipur, Bijnor Changipur (J.R.F.) Sample Collected By: Mr. S.K. Tripathi (S.A.), Subash Chandra (J.R.F.)

4-

Source of Sampling: 25 TPH Boiler Stack attached to: 25 TPH Boiler

6-

Stack Height: 72 mtr Total No. of Boiler: 01

8-

5-

Capacity of Boiler: 25 TPH

9-

10-

Fuel used: Baggasse, slop

11-

Quantity of Fuel used: 94 ton Baggasse and 288 ton slop

12-

Flue Gas Velocity: 8.4 m/s

13-

Air Pollution Control Device: ESP

Other remarks (if any): -14-

Further details of sample location and Test methods followed are appened overleaf:

Sr no.	Parameter	Unit	Result	Standards
1	Particulate matter	mg/Nm3	44	50mg/Nm3
2	Sulphur dioxide	mg/Nm3	22	600mg/Nm3
3	Oxide of Nitrogen	mg/Nm3	64	300mg/Nm3

Note: The results in the Test Report relate only to the items tested. The Report shall not be reproduced-except in Full, without the written permission of laboratory.

[Abhishek Rajput JRF]

Authorised Signatory-



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TEST REPORT

Amekwe Mo. 2 page No.: 1 of 2

TEST REPORT No. NCL/ED-014/28/02/25 Name and Address of Customer

DATE OF REPORT : 03/03/2025

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changipur, District - Bijnor

Sample Name

SAMPLING DETAIL : AMBIENT AIR

Analysis Start Date

28/02/2025

**Date of Sampling** Time of Sampling

Sampling Protocol

: 27/02/2025

: 10:00 AM (27/02) TO 10:00 AM (28/02)

: IS:5182

Sampling Flow Rate for : 0.5 LPM Gases

Sampling Duration **Equipments Used** 

Ambient Temperature

24 Hrs

Sample ID No.

Analysis End Date

Sampling Done By

Sampling Location

: NCL/ED-014/28/02/25

: NCL

: 03/03/2025

: Near Stockyard

Sampling Flow Rate of SPM : 1.26 Mtr /min (Average)

Sampling Machine Placed at : 3.0 Mtr Height (from ground)

Respirable Dust Sampler (PM10)+Fine Particulate Sampler (PM2.5) With Gaseous Attachment

: 27°C

PHYSICAL OBSERVATIONS

Wind Direction

: East to West

Weather Conditions Clear

#### **TEST RESULT**

S.No.	Test Parameters	Units	Test Method	Results	Specification As
1	Particulate Matters (Size Less Than 10µm) (PM10)	µg/m3	IS:5182 (Part 23)	80	For 24 Hrs=100
2	Particulate Matters (Size Less Than 2.5µm) (PM2.5)	µg/m3	NCL/AIR/STP-09	42	For 24 Hrs=60
3 .	Sulphur Dioxide (SO2)	µg/m3	IS:5182 (Part 2)	17.6	For 24 Hrs=80
4	Carbon Monoxide (CO)	mg/m3	IS:5182 (Part 10)	0.61	For 08 Hrs=02 For 1 Hrs =04
5	Nitrogen Dioxide (NO2)	µg/m3	IS:5182 (Part 6)	31.4	For 24 Hrs=80
	Lead (Pb)	µg/m3	IS:5182 (Part 22)	BDL(DL-0.05)	For 24 Hrs=1.0
	Ozone (O3)	µg/m3	IS:5182 (Part-9)	20.5	For 8 Hrs=100 For 1 Hr=180
	Ammonia (NH3)	µg/m3	NCL/AIR/STP-13	BDL(DL-20.0)	For 24 Hrs=400
	Benzene (C6 H6)	µg/m3	IS:5182 (Part-11)	BDL(DL-1.0)	For Annual=05
0	Benzo (a) Pyrene (BaP)	ng/m3	IS:5182 (Part-12)	BDL(DL-0.1)	For Annual=01



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Authoriz

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Mobile: 9810430345/9205501788 | Website: www.newconlab.in

E-mail: newconlab@gmail.gop. 199/conlab@gmail.com



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TEST REPORT No. NCL/ED-014/2

Page No.: 2 of 2

	314/28/02/25		DATE OF REPORT : 03/0:				
Test Para  11 Arsenic (As)	Imeters Units	Test Method	Results	Specification As per CPCB			
Nickel (Ni)	ng/m3	NCL/AIR/STP-19	BDL(DL-1.0)	For Annual=06			
Remarks: BDI - D.	ng/m3	NCUAIR/STP-17	BDL(DL-5.0)	For Annual=20			

)L=Below Detection Limit.

\*\*\*End of Report\*\*\*





Arvind Phoudhary

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E-mail: newconlab@gmail.com, newconlabfinance@gmail.com



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TEST REPORT No. NCL/ED-013/28/02/25 Name and Address of Customer

TEST REPORT

Page No.: 1 of 2

DATE OF REPORT : 03/03/2025 M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changipur, District - Bijnor

Sample Name

Analysis Start Date : AMBIENT AIR

Date of Sampling : 28/02/2025 Time of Sampling

: 27/02/2025

Sampling Protocol

Sampling Flow Rate for : 0.5 LPM

Sampling Duration : 24 Hrs

**Equipments Used** 

SAMPLING DETAIL

Analysis End Date

: 10:00 AM (27/02) TO 10:00 AM (28/02) Sampling Location Sampling Done By

: Near Boiler Area

: NCL/ED-013/28/02/25 Sample ID No. Sampling Flow Rate of SPM : 1.27 Mtr3/min

(Average) Sampling Machine Placed at : 3.0 Mfr Height (from ground)

: Respirable Dust Sampler (PM10)+Fine Particulate Sampler (PM2.5) With Gaseous Attachment PHYSICAL OBSERVATIONS Wind Direction

Ambient Temperature : 27°C Weather Conditions : Clear

: East to West

: 03/03/2025

: NCL

S.No	. Test Parameters	TES	T RESULT		
		Units	Test Method	Results	Specification As
1	Particulate Matters (Size Less Than 10µm)	-			per CPCB
		µg/m3	IS:5182 (Part 23)	84	For 24 Hrs=100
2	Particulate Matters (Size Less Than 2.5µm)	+			
	[ · · · · · · · · · · · · · · · · · · ·	ha/w3	NCL/AIR/STP-09	45	For 24 Hrs=60
3	Sulphur Dioxide (SO2)				
4	Carbon Monoxide (CO)	µg/m3	IS:5182 (Part 2)	18.1	For 24 Hrs=80
	(60)	mg/m3	IS:5182 (Part 10)	0.64	
5	Nitrogen Diaxide (NO2)			0.04	For 08 Hrs=02 For 1 Hrs =04
3		µg/m3	IS:5182 (Part 6)	32.2	
	(-)	µg/m3	IS:5182 (Part 22)		For 24 Hrs=80
	Ozone (O3)	µg/m3		BDL(DL-0.05)	For 24 Hrs=1.0
		Pyrins	IS:5182 (Part-9)	20.8	For 8 Hrs=100 For 1
	Ammonia (NH3)	unt-0			Hr=180
1	Benzene (C6 H6)	µg/m3	NCL/AIR/STP-13	BDL(DL-20.0)	For 24 Hrs=400
_		µg/m3	IS:5182 (Part-11)	BDL(DL-1.0)	
	Benzo (a) Pyrene (BaP)	ng/m3	IS:5182 (Part-12)		For Annual=05
/28/02 1-8:- [	- 1		15.5102 (Fall-12)	BDL(DL-0.1)	For Annual=01

ED-013/28/02/25-1

Section thicharge Checked by

Choudhary

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 Endorsement of the same is neither inferred nor impl
 Laboratory shall maintain the confidentiality of all inf
 Complaints about this report should be communicate
 The report is not to be produced wholly or in part with Il information related to the sa icated within 10 days of the iss t without prior permission of the

the samples & test reports.

the issue date of this report,
an of the Managing Partner, All disputes subject to Ghaziabad Aurisdiction.

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E-mail: newconlab@gmail.com/newconlabfinance@gmail.com



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# TEST REPORT No. NCL/ED-013/28/02/28

Page No.: 2 of 2

BDL(DL-5.0)

S.No.			DATE OF REF	ORT :03/03/2025
Test Parameters  11 Arsenic (As)	Units	Test Method	Results	Specification As per CPCB
(Ni)	ng/m3	NCL/AIR/STP-19	BDL(DL-1.0)	For Annual=06 For Annual=20
Rom	mate. a		DOL/DI-50)	1017

ng/m3

Remarks: BDL=Below Detection Limit.

\*\*\*End of Report\*\*\*

NCL/AIR/STP-17





Arvill Choudhary

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**TEST REPORT** 

Armexure Mo. 3 page No.: 1 of 1

TEST REPORT No. NCL/ED-015/28/02/25 Name and Address of Customer

DATE OF REPORT : 03/03/2025

M/S BINDALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changipur, District - Bijnor

Sample Name

SAMPLING DETAIL

Analysis Start Date

: Ambient Noise

28/02/2025

Analysis End Date

: 28/02/2025

Date of Monitoring Monitoring Duration

: 27/02/2025

: 24 Hrs

Monitoring Done By Place of Monitoring

Protocol

: NCL : Near Boiler Area

Time of Monitoring

: 10:30 AM (27/02) TO 10:30 AM (28/02)

NCL/AIR/STP/20

Category of Area

: Industrial Area

OBSERVATIONS								9 10	
1	2	3	4	5	6	7	8	9	
62.8	63.3	63.9	64.2	64.5	65.1	65.6	66.2	66.7	67.4
52.7	52.2	53.0	543	54.9	55.2	55.6	56.1	56.7	57.2
	1 62.8 52.7	1 2 62.8 63.3	1 2 3 62.8 63.3 63.9	1 2 3 4 62.8 63.3 63.9 64.2	1 2 3 4 5 62.8 63.3 63.9 64.2 64.5	02.0 03.3 03.9 04.2 04.0	1 2 3 4 5 6 7 62.8 63.3 63.9 64.2 64.5 65.1 65.6	1 2 3 4 5 6 7 8 62.8 63.3 63.9 64.2 64.5 65.1 65.6 66.2	1 2 3 4 5 6 7 8 9 62.8 63.3 63.9 64.2 64.5 65.1 65.6 66.2 66.7

#### TECT DECLII T

S.No.	Test Parameter	Results	Specification As Per CPCB
D		Results	
	Time Noise Level		
1	Average Noise Level	65.0	
2	L Max	67.4	
3	L Min	62.8	-
4	Day Leq	65.2	75.0 Max
Nigh	t Time Noise Level		
5	Average Noise Level	55.0	
3	L Max	57.2	
7	L Min		
3	Night Leq	52.7	
	mgir Led	55.2	70.0 Max

\*\*\*End of Report\*\*\*

Remarks: >Day time reckoned between 6:00AM To 10:00PM.

>Night time reckoned between 10:00PM To 06:00AM.

ED-015/28/02/25-1

ar & Die

FOR NEWPON CONSULTANTS & LABORATORIES

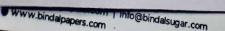
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TEST REPORT

Page No.: 1 of 1

DATE OF REPORT : 103/03/2025

TEST PERFORT IN, WOLED-VINDONICS

Name and Address of Contomer

MAS EMICIALS PAPERS MILLS LTD. (SUGAR UNIT)

Village - Changiour, District - Bijnor

SAMPLING DETAIL

Sarryla Harris

; Ambient Noise

Analysis End Date

: 28/02/2025

Arshipse Start Date

: 201500025

Monitoring Done By

: NCL : Near Stockyard

Date of Ministry Montecking Duration

: 27/10/2025 : 24 Hrs

Place of Monitoring

: NOLIAIRISTPIZO

Time of Monitoring

: 10:30 AM (27/02) TO 10:30 AM (28/02) Protocol

CAMPBORY OF HISS

; Industrial Area

**ORSERVATIONS** 

Observation No.	1	2	3	4	-	662	66.7	57.2	67.7	68.1
Day Time Reading (DSIA)	63.6	64.1	84.5	65.3	65.9			56.8	57.1	57.6
High Time Passing (GEI/A)	52.8	53.4	54.1	54.7	55.3	55.9	30.2			

#### TEST RESULT

	IEST NEGOE.	Specification As Per CPCB
No. Test Parameter	Results	
Day Time Noise Level	65.9	
1 Average Noise Level	68.1	
2 L Max	63.5	
3 Littin	66.1	75.0 Max
4 Day Leg		
Night Time Noise Level	55A	
Average Noise Level	57.8	
L Max	52.8	
L Min	56.8	70.0 Max
Hight Led	SARENA OF RESERVED	

Remarks: >Day time reckoned between 6:00AM To 10:00PM.

>Night time reckoned between 10:00PM To 06:00AM.

ED-016/28/02/25-1



charge

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